

# Prediction of Contaminant Retention and Transport in Soils Using Kinetic Multireaction Models

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Mathematical models that describe the retention reactions of contaminants in the soil system are presented. Single and multireaction-type models for simultaneous retention and transport in the soil profile are discussed. Single retention models are classified into two types: equilibrium and kinetic models. Emphasis is given to the nonlinearity and kinetic behavior of solute retention processes in soils. Two-site models that include the equilibrium-kinetic types as well as the fully kinetic type are also examined. A multireaction-type model is also presented, which includes reversible and irreversible retention processes of the equilibrium and kinetic types. Advantages of the multireaction approach over the single or two-site models are discussed. The predictive capability of the two-site model and the multireaction model for their description of experimental results for phosphorus and two heavy metals (Cd and Cr) are examined.

## Introduction

Retention reactions that occur in the soil are important processes that govern the fate of chemical contaminants and hazardous chemicals in groundwater. Mathematical models that describe the potential mobility of dissolved chemicals must therefore include the physical and chemical, as well as biological, processes that influence the behavior of these chemicals in the soil matrix. The ability to predict the mobility of dissolved chemicals in the soil and the potential contamination of groundwater supplies is important in assessment of hazards and is a prerequisite for the management of land disposal of chemicals contaminants.

In this paper, a review of widely used solute retention models is presented. Emphasis is on solute retention mechanisms characterized by time-dependent (or kinetic) and nonlinear type reactions. Several multireaction models for the transport and retention of contaminants are presented.

## Equilibrium Retention Models

It is well accepted that, under steady water flow conditions, transport of dissolved chemicals in soils is governed by the following convection-dispersion transport equation (1):

$$\rho \frac{\partial s}{\partial t} + \theta \frac{\partial c}{\partial t} = \theta D \frac{\partial^2 c}{\partial x^2} - q \frac{\partial c}{\partial x} - Q \quad (1)$$

where  $c$  is the concentration of the dissolved chemical in the soil solution (mg/L) and  $s$  is the amount of solute retained per unit mass of the soil matrix (mg/kg). In addition,  $D$  is the hydrodynamic dispersion coefficient ( $\text{cm}^2/\text{day}$ ),  $q$  is the Darcy water flux ( $\text{cm}/\text{day}$ ),  $\theta$  is the volumetric soil moisture content ( $\text{cm}^3/\text{cm}^3$ ),  $\rho$  is the soil bulk density ( $\text{g}/\text{cm}^3$ ),  $t$  is time (day) and  $x$  is soil depth (cm). The two terms on the right-hand side of Eq. (1) are commonly known as the dispersion and convection terms, respectively. The term  $(\partial s/\partial t)$  represents the rate for reversible solute removal from the soil solution. In contrast, the term  $Q$  is a source or a sink representing irreversible solute production ( $Q$  negative) or solute removal ( $Q$  positive) from the soil solution ( $\text{mg}/\text{cm}^3 \cdot \text{day}$ ).

Over the last 2 decades, several analytical models for the description of solute transport in porous media have been proposed. One group of models deals with solute transport in well-defined geometrical systems of pores and/or cracks of regular shapes or interaggregate voids of known geometries. Examples of such models include those of Rao et al. (2), Rasmuson and Neretnieks (3) (for uniform spheres), Tang et al. (4) (for rectangular voids), van Genuchten et al. (5) (for cylindrical voids), and Rasmuson (6) (for discrete aggregate or spherical size geometries). van Genuchten and Dalton (7) provided a review of models using such an approach. Solutions of these models are analytic, often complicated, and involve several numerical approximating steps. Recent applications include transport in fixed beds consisting of spheres or aggregates (8,9). Another group of transport models that are widely used are those that do not consider well-defined geometries of the pore

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space or soil aggregates. Rather, solute transport is treated on a macroscopic basis with  $\rho$ ,  $\theta$ ,  $q$ , and  $D$  of Eq. (1) as the associated parameters that describe the transport processes in the bulk soil. The mobile-immobile transport models are refinements of this macroscopic approach. Here, it is assumed that soil-water is divided into two regions. A mobile-water region is one that is considered to be present in large pores and through which solute transport occurs by convection and mechanical dispersion. The other is an immobile-water region present in the bulk matrix and through which relatively low or no water flows. Mobile-immobile models have been introduced by Coats and Smith (10), Skopp and Warrick (11), van Genuchten and Wierenga (12), and Skopp et al. (13). The mobile-immobile models have been extensively used to describe several solutes [for a review see Nielsen et al. (14)].

Description of the solute retention mechanisms as expressed by the term  $(\partial s/\partial t)$  has been the focus of investigators for several years. Such a description, when incorporated into Eq. (1), provides a predictive tool for the transport of dissolved chemicals in the soil profile. Most mathematical models that describe the retention mechanisms are based on the validity of the local equilibrium assumption (LEA) in the soil system (15). Here one assumes that the reaction of an individual solute species in the soil is sufficiently fast or instantaneous and that an apparent equilibrium condition may be observed in a few minutes or hours. Such a behavior has been used as the basis for soil surface adsorption mechanisms as well as ion-exchange reactions. Illustrative examples of equilibrium-type solute retention are shown in Figure 1. The data are from kinetic batch experiments of Mg retention by a Ca saturated Abist soil and for two aggregate size separates. The time of reaction does not appear to be significant. No apparent change in Mg concentration occurred after 4 hr of reaction. Such rapid retention reactions or equilibrium solute behavior has been observed for other solutes (16–18).

Linear, Freundlich, and Langmuir sorption models are perhaps the most commonly used equilibrium-type models for describing the retention of a wide range of dissolved chemicals in soils. A partial listing of equilibrium type models are given in Table 1. The linear and Freundlich models use the solute distribution coefficient ( $K_D$ ), which partitions the solute between that in the soil solution and the amount sorbed by the soil matrix. A discussion of the  $K_D$  parameter and its capability for describing contaminant migration is given by Reardon (19). Unlike the Langmuir models, linear and Freundlich models do not include a maximum sorption term ( $s_{\max}$ ). This is disadvantageous since the capacity of the soil for solute removal, i.e., the total sites, is finite and should be an important limiting factor.

Langmuir models are perhaps the most widely used equilibrium models for describing the fate of solutes such as phosphorus and heavy metals in soil (18,20,21). The two-site Langmuir model may be considered as one of the earliest multireaction type models. Here one as-

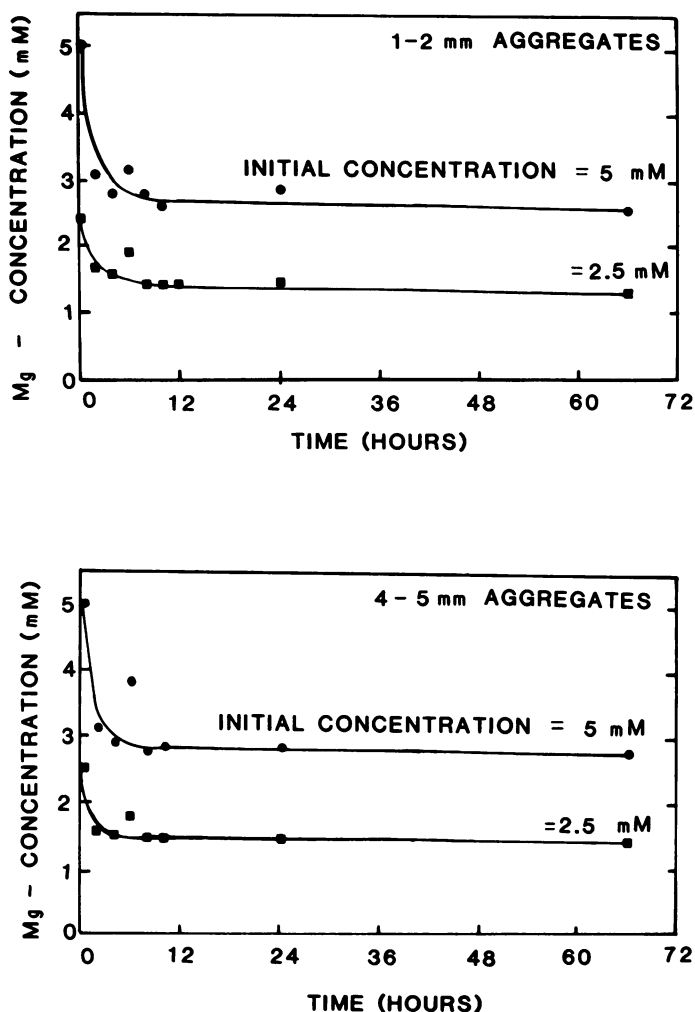


FIGURE 1. Mg concentration vs. time of reaction from batch kinetic experiments for two aggregate sizes of Abist (Aquic Eutrochrept) soil (15).

Table 1. Fast or equilibrium type models for contaminant retention in soils.

Model	Formulation
Linear	$s = K_D c$
Freundlich (nonlinear)	$s = K_D c^n$
Langmuir	$s = bcs_{\max}/[1 + bc]$
Langmuir with sigmoidicity	$s = bcs_{\max}/[1 + bc + k/c]$

sumes complete equilibrium and partitions the reaction sites into two fractions. Holford et al. (22) were one of the earliest researchers to evaluate this model for describing P retention by several soils.

Recently, the two-site Langmuir was modified to incorporate the sigmoidal shape of Cu, Pb, and Cd sorption isotherms observed at extremely low concentrations (23). The equilibrium models given in Table 1 have been used to describe adsorption isotherms for a wide range of solutes including major cations (Na, Ca, Mg, and K), heavy metal species, and organics (16,24). How-

ever, as pointed out by Veith and Spósito (25) and Spósito (26), a good fit of a particular adsorption isotherm does not in itself constitute a proof of any specific sorption mechanism.

Other types of equilibrium models are those based on ion-exchange reactions (27,28). Unlike the previous models, which are empirical in nature, ion-exchange models are based on rigorous thermodynamics in which the reaction stoichiometry is explicitly considered. A set of recursion formulae has been formulated by Rubin and James (27) that describe exchange isotherms for multiple ions in the soil. Recently, aqueous equilibrium reactions, along with ion-exchange reactions, have been used to describe multiple ion transport in soils (29,30). Ion exchange has been used by several researchers to describe the transport of cations present in the soil solution (28,31-33).

## Kinetic Retention Models

It has been observed that the amount of solute retained (or released) from the soil solution may be strongly time dependent. Selected examples of kinetic retention for Cd are given in Figure 2. Here, the kinetic dependence of Cd reactions, carried out in batch experiments, is shown for various soils (24). The amount of Cd retained varied among soils with Cecil soil exhibited the lowest retention, whereas the Sharkey soil showed maximum Cd retention. The sharp decrease in Cd concentrations indicates a fast-type sorption reaction, which was followed by slower type reactions. It is

also apparent that even after 300 hr, quasi-equilibrium conditions were not attained. The results shown in Figure 3 illustrate the influence of kinetic reactions on the shape of sorption isotherms of P in a Norwood soil. The amount of P sorbed increased with time as well as with concentration. It is apparent that the use of equilibrium-type models would yield inadequate predictions of the fate of such solutes in the soil system.

Several models have been proposed to describe the kinetic reactions of dissolved chemicals in the soil solution. Most common is the first-order kinetic reaction, which was incorporated into the convection-dispersion transport equation by Lapidus and Amundson (34). Such reactions are assumed to be fully reversible, and the magnitude of the reaction coefficients determines the time when apparent equilibrium may be attained. The use of such linear models has been rather restricted due to the nonlinear behavior of most solute retention reactions, exemplified by the cases shown in Figures 2 and 3. The first-order kinetic model has been modified to account for the nonlinear-kinetic behavior of retention mechanisms. Such a modified model was used successfully for describing the retention of P and several pesticides in batch and miscible displacement studies (16,35). Another fully reversible model is that of the Langmuir kinetic type (Table 2). Important features of this kinetic model are that it includes a maximum re-

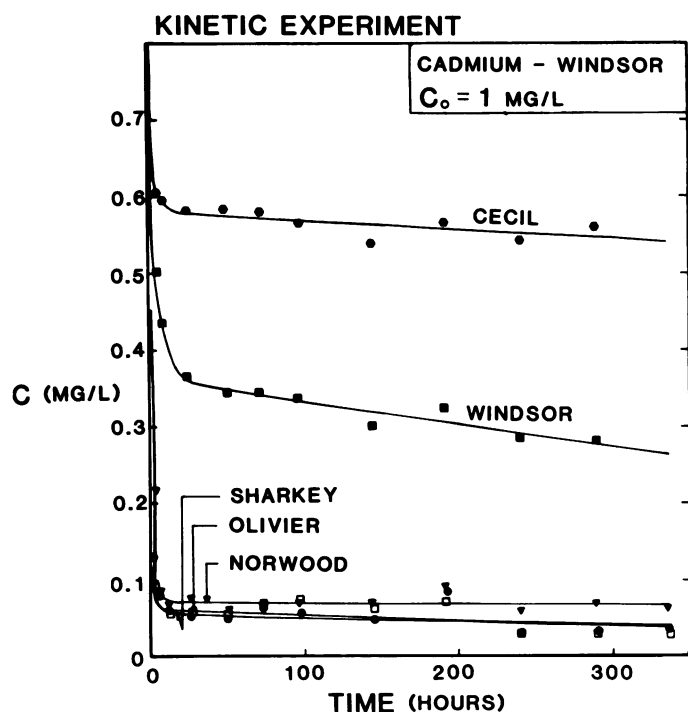


FIGURE 2. Cd concentration vs. time of reaction for five soils (16).

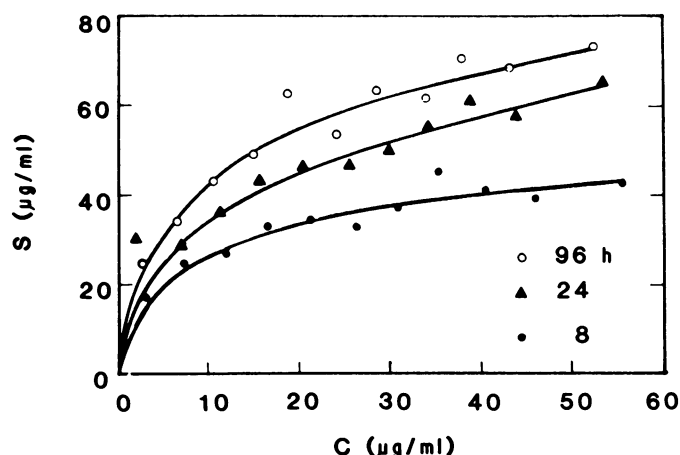


FIGURE 3. P sorption isotherms after 8, 24, and 96 hr of reaction time for a Norwood soil. Solid curves are predictions using the nonlinear Freundlich model.

Table 2. Insufficiently fast or kinetic-type models for contaminant retention in soils.

Model	Formulation
First-order	$\partial s / \partial t = k_1 (\Theta / \rho) c - k_2 s$
Nth order	$\partial s / \partial t = k_1 (\Theta / \rho) c^n - k_2 s$
Irreversible (sink/source)	$\partial s / \partial t = k_s (\Theta / \rho) (c - c_p)$
Langmuir kinetic	$\partial s / \partial t = k_1 (\Theta / \rho) c (s_{\max} - s) - k_2 s$
Elovich	$\partial s / \partial t = A \exp(-Bs)$
Power	$\partial s / \partial t = k_1 (\Theta / \rho) c^n s^m$
Mass transfer	$\partial s / \partial t = k (\Theta / \rho) (c - c^*)$

tention capacity term and that it is nonlinear in nature (15). A discussion of the kinetic behavior of the Langmuir sorption reaction mechanisms during transport is presented by Jennings and Kirkner (36).

## Multireaction Kinetic Models

A widely used multireaction model is the two-site model proposed by Selim et al. (37) and Cameron and Klute (38). This model was developed for the purpose of describing observed batch results, which showed rapid initial retention reactions followed by slower type reactions. The model was also developed to describe the excessive tailing of breakthrough results obtained from pulse inputs in miscible displacement experiments. Single retention models of the first and  $n$ th-order kinetic type failed consistently to describe such batch or miscible displacement results. The two-site model is based on several simplifying assumptions. It is assumed that a fraction of the total sites (referred to as type I sites) are highly kinetic in nature. As a result, type I sites were assumed to react slowly with the solute in the soil solution. In contrast, we consider type II sites to react rapidly with soil solution. The retention reactions for both types of sites were based on the nonlinear (or  $n$ th order) reversible kinetic approach as outlined in Table 2. The convection-dispersion transport equation with the two-site retention mechanism may be expressed as:

$$\theta \frac{\partial c}{\partial t} = \theta D \frac{\partial^2 c}{\partial x^2} - q \frac{\partial c}{\partial x} - (k_1 \theta c^n - k_2 \rho s_1 - (k_3 \theta c^m - k_4 \rho s_2)) \quad (2)$$

$$\frac{\partial s_1}{\partial t} = k_1 \left[ \frac{\theta}{\rho} \right] c^n - k_2 s_1 \quad (3)$$

$$\frac{\partial s_2}{\partial t} = k_3 \left[ \frac{\theta}{\rho} \right] c^m - k_4 s_2 \quad (4)$$

$$s_t = s_1 + s_2 \quad (5)$$

where  $s_1$  and  $s_2$  are the amounts retained by sites I and sites II, respectively, and  $s_t$  is the total amount of solute retained. The nonlinear parameters  $m$  and  $n$  are usually considered less than unity and  $n \neq m$ . For the case  $n = m = 1$ , the retention reactions are of the first-order type, and the problem becomes a linear one. This two-site approach was also considered for the case when type II sites are assumed to be in equilibrium with the soil solution. Such conditions may be attained when the values for the forward and backward (or  $k_3$  and  $k_4$ ) rate coefficients are extremely large in comparison to the water flow velocity ( $q$ ); that is, the local equilibrium assumption is valid for type II sites (39). Under these conditions, the solute convection-dispersion transport equation for a combined model of equilibrium and kinetic retentions is (37):

$$R \frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2} - v \frac{\partial c}{\partial x} - (k_1 c^n - k_2 \left[ \frac{\rho}{\theta} \right] s_1) \quad (6)$$

$$R = 1 + \left[ \frac{\rho}{\theta} \right] K_D m c^{m-1} \quad (7)$$

$$s_2 = K_D c \quad (8)$$

where Eqs. (7 and 9) describe equilibrium reaction of the Freundlich type. The term  $R$  of Eq. (7) is the retardation factor which for this nonlinear case is a function of  $c$ . Selim et al. (18) found that the use of the equilibrium and kinetic two-site model provided improved predictions of breakthrough curves (BTCs) for Picloram in soils. This result was due primarily to improved predictions of the excessive tailing of the desorption or leaching side and the sharp rise of the sorption side of the BTCs in comparison to predictions using single reaction equilibrium or kinetic models. Examples of predictions for two pesticides using this model are shown in Figure 4. Here, atrazine and (2,4-dichlorophenoxyacetic acid) were applied as separate pulses into different soil columns. The equilibrium and kinetic two-site model described in BTCs adequately for both pesticides and for different input pulse concentrations ( $c_0$ ). In order to obtain the predictions shown in Figure 4, it was necessary that the retention reactions for the equilibrium and the kinetic sites were nonlinear with the values for  $m$  and  $n$  less than unity.

The two-site model has been used by several scientists including De Camargo et al. (40), Rao et al. (41), Hoffman and Rolston (42), Jardine et al. (43), Nkedi-Kizza et al. (8), and Parker and Jardine (44), among others. The model proved successful in describing the retention and transport of several dissolved chemicals, including aluminum, 2,4-D, atrazine, phosphorus, potassium, cadmium, chromium, and methyl bromide.

Major disadvantages of the two-site model are that it is restricted to reversible mechanisms and that it does not account for possible consecutive-type solute interactions in the soil system. Several multireaction models have been introduced to incorporate irreversible as well as reversible reactions of the concurrent or the consecutive type. An example of a multireaction model is shown by the schematic diagram of Figure 5. Here we consider the solute to be present in the soil in five phases:  $c$ ,  $s_1$ ,  $s_2$ ,  $s_3$ , and  $s_s$ . It is assumed that the rate of irreversible reaction ( $\partial s_s / \partial t$ ), which is equivalent to the sink term  $Q$  of Eq. (1), can be expressed as

$$Q = \rho \frac{\partial s_s}{\partial t} = \theta k_s c \quad (9)$$

This is a first-order irreversible kinetic process, and  $k_s$  is the associated rate coefficient (per day). Mansell et al. (35) proposed this approach for describing possible precipitation of P in miscible displacement studies. Fiskell et al. (45) found that incorporation of  $s_s$  in the model

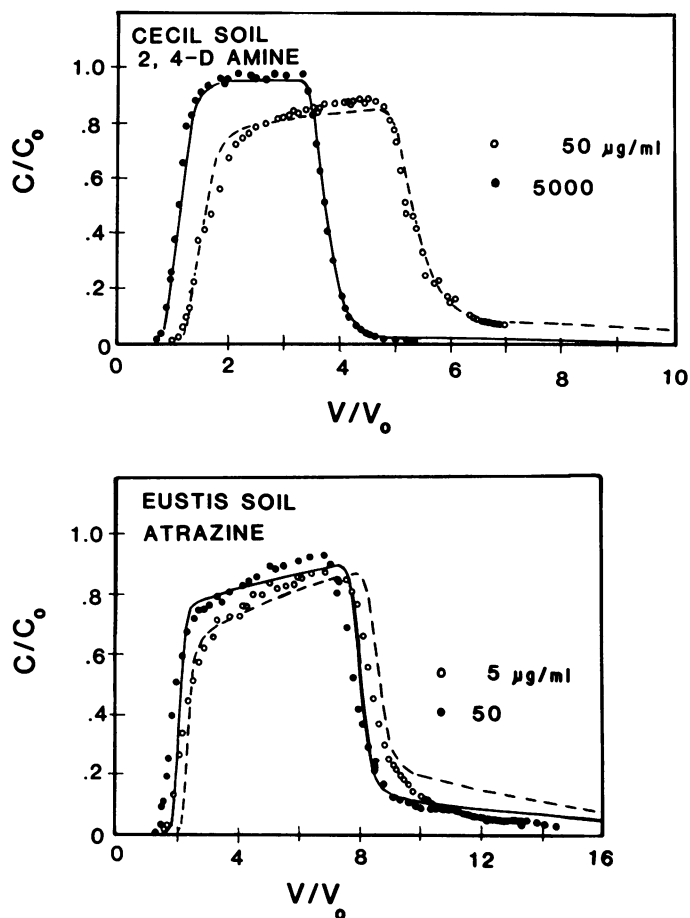


FIGURE 4. Breakthrough curves for 2,4-D amine and atrazine for two pulse concentrations. Dashed and solid curves are predictions using the two-site model (21).

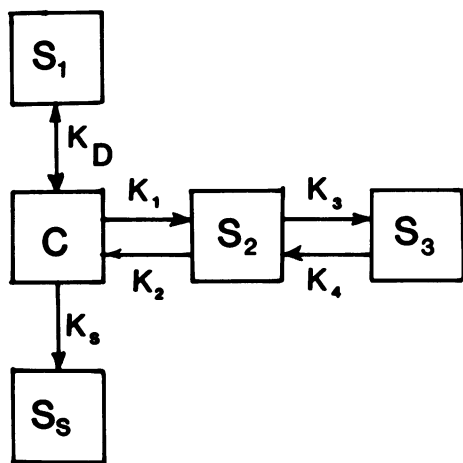


FIGURE 5. A schematic diagram of a multireaction model for solute retention in the soil system.

was essential in describing the slow P retention kinetics for a Spodosol from deep and shallow tilled treatments. Recently, Amacher et al. (18) showed that the sink term was necessary to describe batch results for Hg, Cd, and Cr retention versus time for five different soils. This sink term is similar to that for diffusion-controlled precipitation reaction if one assumes that the equilibrium concentration for precipitation is negligible and that  $k_s$  is related to the diffusion coefficient. Among kinetic models that are used to describe the rate of irreversible reactions is the Elovich model given in Table 2. For further discussion of irreversible kinetic models see Travis and Etnier (16).

As indicated by Figure 5, the  $s_1$  and  $s_2$  phases are in direct contact with  $c$ , and reversible processes of the equilibrium and kinetic types govern their reactions, respectively. The  $s_1$  and  $s_2$  phases may be regarded as the amounts adsorbed on surfaces of soil particles as well as chemically bound to Al and Fe oxides surfaces or other type surfaces. Moreover, these phases may be characterized by their fast sorption from, as well as release to, the soil solution and, thus susceptibility to leaching in the soil. In contrast,  $s_3$  is considered here as the amount which is nonlabile, firmly held, or fixed by the soil matrix. Furthermore, this phase may be characterized by its slow (retention and release) reactions. Therefore, it is often assumed that the firmly held phase is less readily available to uptake by plant roots or transport in the soil profile.

The predictive capability of the multireaction model above was tested for two different solutes [P and Cr(VI)] and for various soils. As illustrated by the BTCs shown in Figures 6 and 7, the model is capable of describing the behavior of these solutes adequately. Such agreement may be regarded as adding credence to the validity of the model. For P predictions, we found that the presence of a consecutive reaction (or  $s_3$ ) was necessary in order to describe the results shown. Moreover, the use of a simple first-order reaction to describe the

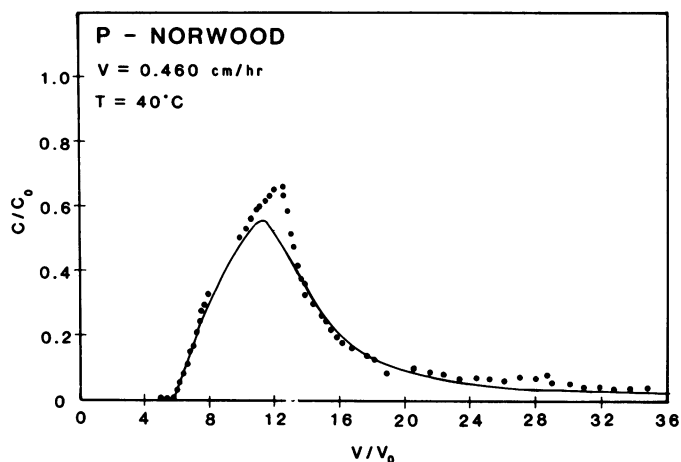


FIGURE 6. Breakthrough for P in a Norwood soil. Solid curve is the prediction using the multireaction model.

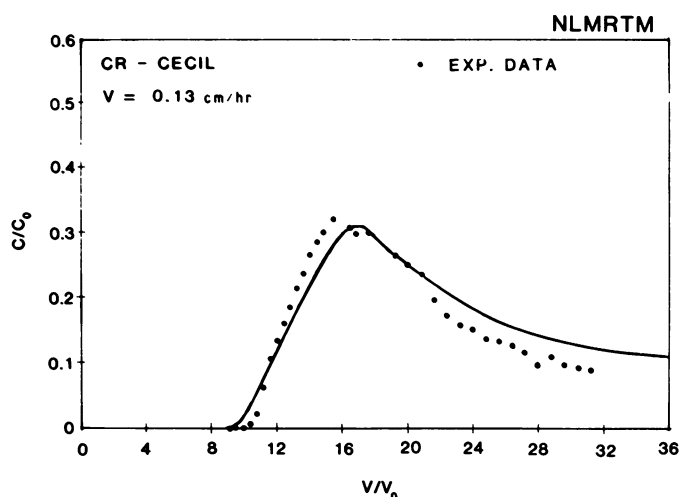


FIGURE 7. Breakthrough for Cr(VI) in a Cecil soil. Solid curve is the prediction using the multireaction model.

slow kinetic retention of the consecutive type reaction in the following form

$$\frac{\partial s_3}{\partial t} = k_3 s_2 - k_4 s_3 \quad (10)$$

proved to be adequate. Here,  $k_3$  and  $k_4$  are the associated rates of reaction (per day). The model was equally capable of describing BTCs for Cr(VI) and P from other soils. Additional predictions were also obtained for batch results (not shown) where a wide range of initial concentrations were used in obtaining time-dependent retention isotherms.

The multireaction model of Figure 5 may be regarded as a simplified version of multicomponent models that account for chemical and/or biological reactions of the sequential and concurrent type. Examples of these reactions include precipitation/dissolution, mineralization, immobilization, biological transformations, and radioactive decay, among others. Models that account for first-order kinetic decay reactions include those of Rasmuson (6) and van Genuchten (46). Other examples of this type of model are those that deal with soil nitrogen transformations reactions (47). Other more complex models are those that are based on ion-exchange reactions for multiple ions along with chemical equilibrium reactions in the soil solution. Examples of such models include those of Jennings et al. (29), Miller and Benson (30), and Cederberg et al. (32).

There are several advantages in using multireaction models of the type shown in Figure 5. First, these models are flexible and can be adapted to incorporate other reactions of the reversible or irreversible type. The governing reactions may be kinetic or equilibrium in nature. Furthermore, such models are not restricted to a specific number of solute species with either concurrent or consecutive reactions. However, a prerequisite for the adoption of a multireaction model as a predictive tool is that the model must be validated for a specific contaminant and conditions under considera-

tion. To carry out complete validation of such a model often requires extensive laboratory evaluation of necessary model parameters. The dependence of model parameters on other variables such as pH, temperature, and redox potential must be determined. Moreover, it is necessary that the model be evaluated for a range of soils having different physical and chemical properties. When rigorous validation of the model is not possible, a partial validation based on a limited data set obtained in the laboratory is necessary. Subsequent to laboratory validation, the model should be tested with data sets obtained from the controlled field experiments. Field evaluation often results in several modifications of the model. In some cases, it is perhaps desirable to have more than one model version with each applicable for a specified set of conditions. Although it is often recognized that data sets that are suitable for model validation may not be available, it is essential that partial model validation is performed.

## Summary

An overview of several models that are used for the description of the retention of dissolved chemicals during transport in the soil profile is presented. Single reaction models were classified into equilibrium and kinetic types. In addition, an equilibrium and kinetic two-site model of the nonlinear type was presented. Major advantages of this combination type model over the single reaction approach were outlined and several solute breakthrough curves illustrated. Furthermore, a generalized form of a multireaction kinetic model was given. The major feature of multireaction kinetic models is that they are flexible, being neither restricted by the number of solute species present in the soil system nor by the governing retention reaction mechanisms. Such models may include reversible and irreversible reactions of the linear and nonlinear kinetic types. Moreover, these models can incorporate concurrent as well as consecutive-type retention reactions that may be equilibrium or kinetic in nature. Rigorous validation of such models is needed for various contaminants and for soils having different physical and chemical properties. Model validation is a prerequisite step before model adoption as a predictive tool of the potential mobility of contaminants in soils.

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